

1 **Laboratory and Field Test and Distinct Element Analysis of Dry Granular flows and**
2 **segregation process**

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9 **Abstract**

10 Natural as well as fill slopes are commonly found in Hong Kong, China and many other countries,
11 and slope failures with the subsequent debris flows have caused serious loss of lives and properties
12 in the past till now. There are various processes and features associated with debris flow for which
13 the engineers need to know so as to design for the precautionary measures. In this study,
14 experiments on flume tests, friction tests, deposition tests, rebound tests have been carried out for
15 different sizes of balls to determine the parameters required for the modelling of dry granular flow.
16 Different materials and sizes of balls are used in the flume tests, and various flow pattern and
17 segregation phenomenon are noticed in the tests. Distinct element (DEM) dry granular flow
18 modeling are also carried out for the flow process. It is found that for simple cases, the flow process
19 can be modelled reasonably well by DEM which is crucial for engineers to determine the pattern
20 and impact of granular flow which will leads to further study in more complicated debris flow.
21 From the laboratory tests, large scale field tests and numerical simulations of the single and
22 multiple material tests, it is also found that the particle size will be the most critical factor in the
23 segregation process during granular flow. It is also found from the laboratory tests and numerical
24 simulations that a jump in the flume can help to reduce the final velocity of the granular flow which
25 is useful for practical purposes.

26
27 **Keywords:** flume test, field test, balls, granular flow, distinct element, flow process

28
29 **1- Introduction**

30 The terrain of Hong Kong is hilly. Many slopes (fill, cut and natural slopes) and roads are formed
31 to cope with the rapid development of Hong Kong, China and many other developed cities. Hong
32 Kong has a high rainfall, with an annual average of 2300mm which falls mostly in summer
33 between May and September. The stability of man-made and natural slopes is of major concern to
34 the Government and the public. Landslides and the subsequent debris flows have caused loss of
35 life and significant amount of property damage in the past. In Hong Kong, for the 50 years after

36 1947, and more than 470 people died due to slope failures and debris flow associated with man-
37 made cut slopes, fill slopes and retaining walls.

38 There are many reported serious slope failures and debris flow problems in China in the recent ten
39 years, due to the significant amount of constructions and inadequate stabilization to many
40 temporary or permanent fill or natural slopes. The destructive power of large scale debris flow is
41 well known, and the prevention of slope instability, reduction of debris flow destructive power by
42 the use of rigid, flexible barrier or other means are well practiced in many countries. There are
43 many cases where the slopes fail with subsequent debris flows in Hong Kong and China (Scott
44 and Wang 1997), which have created various serious problems. Based on a conservative estimate,
45 over 60 countries in the world have faced the problems of debris flow over the years. With
46 reference to Fig.1, the debris flows in Hong Kong and China have created traffic problems, **serious**
47 **loss of lives and properties, and currently there are many active research works in the area of debris**
48 **flow in Hong Kong and China. The research works include three-dimensional slope stability**
49 **analysis, debris flow process, impact loads on flexible and rigid barriers and others. An example**
50 **on three-dimensional ~~Morgenstern-Price~~ slope stability analysis using 16000 columns has been**
51 **carried out by Cheng in 2016/2017 which is shown in Fig.2a (Lo et. al. 2018). The analysis of the**
52 **non-spherical surface is achieved by the use of Nurbs function as discussed by Cheng et al. (2005);**
53 **~~and Nurbs representation is a popular method as adopted in many 3D cad programs.~~ Upon the**
54 **determination of the critical failure mass, ~~and~~ the flow path of the soil can be estimated from a**
55 **distinct element analysis using the method as discussed by Cheng et al. (2015). The slope failure**
56 **and the subsequent debris flow (2100m³ of debris) as shown in Fig.2b is finally protected by the**
57 **use of three levels of flexible barrier against the future potential debris flow. ~~The authors are also~~**
58 **~~considering the use of meshless method in the assessment of debris flow, which will be the next~~**
59 **~~stage of the present work (Wong 2018).~~**

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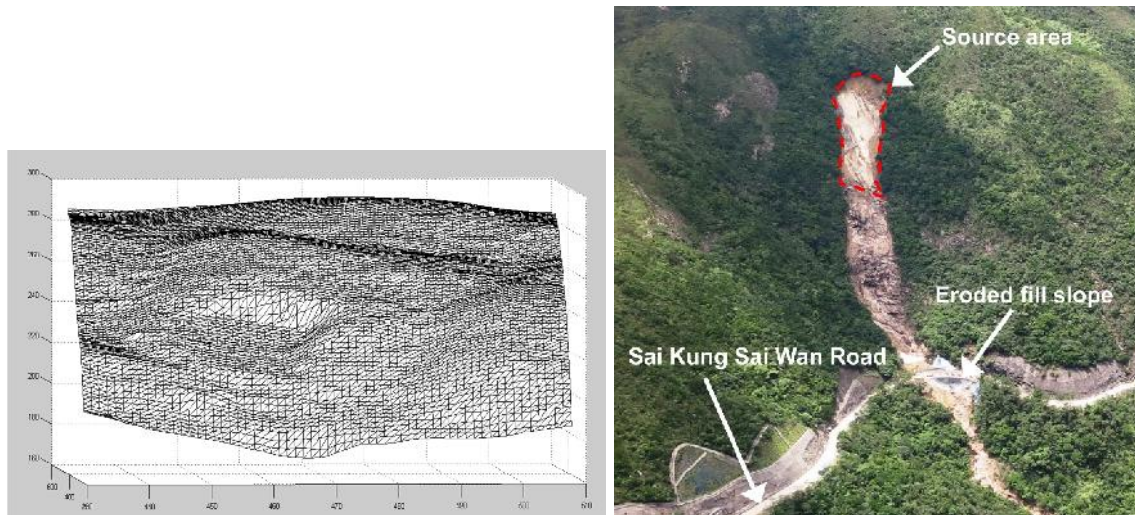


61
62 (a)



(b)

63 Fig.1 Representative debris flow in Hong Kong and Shenzhen, China (a) Tsing Shan debris flow
64 in 1990 (King 2013); (b) debris flow in Shenzhen 2015 (see Wikipedia).



65

66 (a) 3D slope stability analysis

(b) Debris flow after slope failure

67 Fig.2 Three-dimensional slope stability analysis ~~for a slope in Hong Kong~~ by Cheng (the
68 triangulation represent the geometry as defined by the GIS information) **and the subsequent debris**
69 **flow for a slope in Hong Kong has blocked the Sai Wan Road traffic**

70

71 **Granular flow as a pilot study of debris flow** has some fundamental difficulties in the physical tests
72 as well as numerical analysis. In general, various particles sizes will be present in a flow, and the
73 debris mix is usually far from uniform in composition. For physical tests, it is difficulty to apply a
74 representative debris flow mix, and the flow process is further complicated by the presence of
75 water. For numerical simulation, it is virtually impossible to accommodate too much particles in a
76 model, ranging from a very small particle size to cobbles or even boulder in the extreme range.
77 Even if such a numerical model can be established, there will be serious numerical problems if the
78 particles sizes differ too much in the system. **Granular flow** can be induced from gravity, driven
79 by fluid dynamic or from both factors. The classification of debris has been given by Varnes (1978),
80 and later modified by Furuya (1980), Ohyagi (1985), Pierson and Costa (1987), Coussot and
81 Meunia (1996), Cruden and Varnes (1996), Hungr et al. (2001), Takahashi (2001, 2006) and others.
82 A detailed theoretical treatment of dry **granular flow** similar to some of the single material tests in
83 the present study has been given by Takahashi (2014) and will not be repeated here. In this study,
84 we will concentrate mainly on the action of gravity, while the effects of water is under study by
85 the authors **as the next stage of research work**.

86 Many scientists have carried out **granular flow** analysis. Lo (2004) **has compared the** different
87 composition of **granular flow** in landsides in Hong Kong and **examined** the coarse and fine particle
88 concentration. Hutter et al. (2005) **has** considered the flow envelopes and the deposition of the flow.

89 In year 1991, the U.S. Geological Survey has made a large scale flume for detailed experimental
90 tests on debris flows. Mizuyama and Uehara (1983) **have** made a flume which is 20 cm wide and
91 25m long, and the slope angle ranged from 5 degree to 25 degree. Liu (1996) **has** made a 18 cm
92 depth, 16 cm width and 150 cm length flume in Yunnan, China, and the flume inclination can be
93 adjusted from 10 to 34 degrees. Lin (2009) **has** made a 20 cm width 8m length flume with a 2.2 m
94 width 3 m length catchment. There are also various flume tests that have been carried out by
95 various researchers in Hong Kong and many other countries.

96 During the transportation period, segregation occurs when debris starts to flow. Iverson (1997)
97 studied the factors that influence the segregation process. He found that particle size has a great
98 effect on the segregation process, and debris with larger particle size move upward while fine
99 particles go downwards. This phenomenon is the opposite of “normal grading” in which the finer
100 particles are found at the upper layers in the lake or river and large particles rest at the bottom. The
101 main reason for the segregation is kinetic sieving, and finer particle can go through the gaps
102 between particles more easily than the larger particle. Large particles can also be found at the front
103 of the flow because of the relatively high velocity of the larger particles at the upper layer,
104 compared with the finer particles with lower velocity at the lower layer. When a stable contact
105 network for large particle is formed at the free surface, the segregation cease to occur and the balls
106 finally deposit at the catchment area.

107 For distinct element modeling (DEM) of **granular flow**, Jiang et al. (2003) **has** studied the methods
108 of generations of ball in PFC2D (Cundall 1971, 1988, Cundall and Hart 1992, Cundall and Strack
109 1979), namely the expansion method and isotropic compression method. Zohdi (2007), Halsey and
110 Mahta (2002) **have** discussed about the physics of granular flow; the contact model and the limit
111 of the friction coefficient. Sullivan (2011) **has** also compared **between** the theory and computation
112 in distinct element analysis. It is well known that the use of DEM can only provide qualitatively
113 instead of quantitative study up to the present (see also the discussion part), **and most researchers**
114 **adopt DEM for qualitative analysis only.**

115 In the present study, **basie** dry granular flow experiments will be conducted under different
116 conditions using glass and rubber balls for a basic study on the flow process and segregation. Both
117 glass and rubber balls of different diameters have been used in the tests, and combination of
118 different size and materials have also been tried in the tests for the illustration of the segregation
119 problem. The experimental results are also analyzed by distinct element analysis using program
120 PFC2D. It is true that three-dimensional distinct element modelling can be a better tool for the
121 present problems, but the previous experience in three-dimensional distinct element modelling by
122 the authors suggest that the amount of computer time can be significant. For the present study, the
123 flume in both the laboratory and field tests are relatively narrow, and off-track movement of the
124 balls/grains are not major. In view of that, two-dimensional modelling has been adopted in the
125 present study, and good results are actually obtained. The tests are performed at relatively simple
126 condition so that the basic problem of flow and segregation can be studied easily. It should also be
127 mentioned that more than 10 ten thousands photos are taken from the laboratory and field tests,

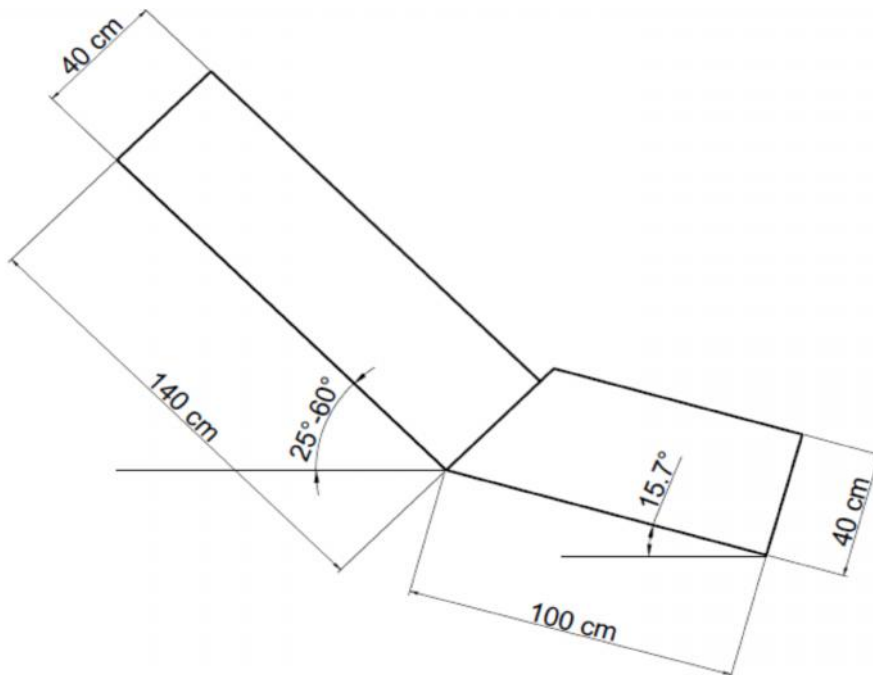
128 and such amount of information cannot be fed into a paper. In views of that, only representative
129 intermediate photos which are used for illustration are given in the present paper, while some of
130 the observed phenomena are simply **description** without the support of the photos.

131

132 2. Physical flume modeling of **granular flow**

133 2.1 Instrumentation and Test Material

134 To enhance the knowledge on the **granular flow** mechanism, many laboratory and large scale field
135 tests have been carried out by the authors. The laboratory model is about 1.5m long and 1.3m high
136 (adjustable). The flume in the laboratory is made of polystyrene and is designed to be flexible, and
137 the angle of inclination can be adjusted if necessary. The flume model is 40cm depth, 40 cm width,
138 140 cm length of upper flume and 100 cm for the lower flume with a 60 x 60 catchment area at
139 the bottom. Fig. 3 and Fig 4 show the schematic design of flume and flume model in the laboratory
140 tests. In order to record the motion of the particles, two high speed cameras are adopted. The first
141 one is mounted on the upper flume **while** the second one is fixed to the bottom flume. In the
142 laboratory tests, different sizes of glass beads and rubber beads are used to replace the use of sand,
143 and this simplification can help to assess the effects of shape and material on the segregation
144 process. In the large scale field test, real sand is used. For the material parameters, the dynamic
145 friction angle is measured by using tilting test (Pudasaini & Hutter (2007), Mancarella & Hungr
146 (2010)). The property of the glass and rubber beads are determined experimentally, and the details
147 are given in Table 1.

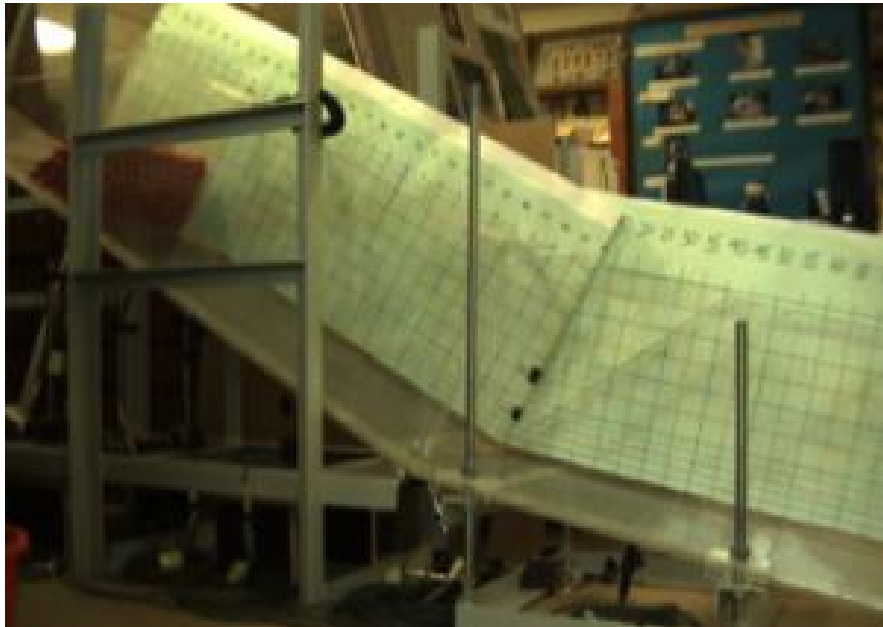


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Fig.3 Schematic Design of Flume

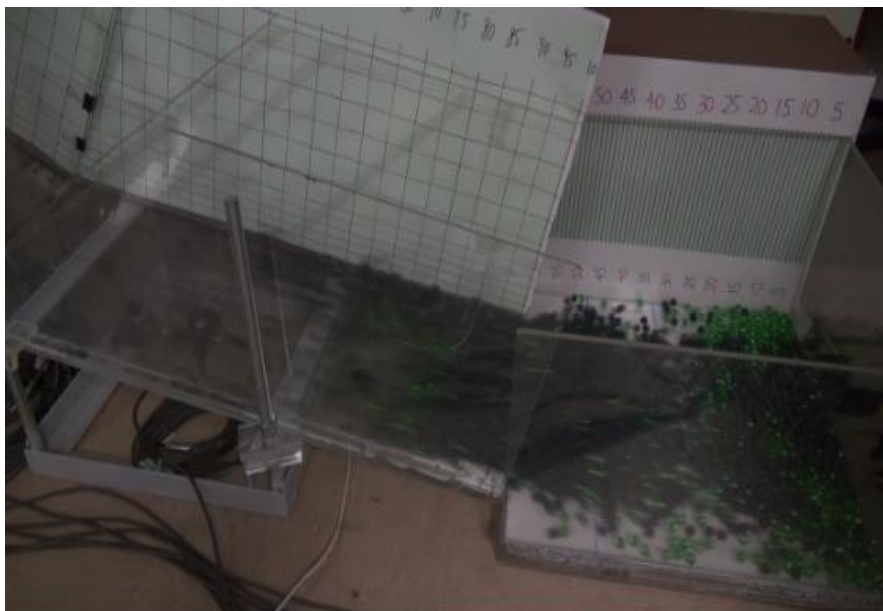
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Fig.4 Flume model in laboratory



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Fig 5. Flume model with a small jump in laboratory



155

156 Fig.6a Transparent glass



Fig.6b Blue glass ball



157

158 Fig.6c Green glass ball



Fig.6d White plastic ball



159

160 Fig.6e Red plastic ball



Fig.6f Black plastic ball

161

162 Table 1. The properties for the glass balls and plastic balls in laboratory granular flow test

Plastic	D(mm)	Average Weight	Density (kg/ m ³)	External Friction Coefficient	Internal Friction Coefficient
White	50	105.35	1609.64	0.781	0.547
Red	30	23.382	1653.97	0.630	0.429
Black	15	2.862	1619.56	0.222	0.365
Glass	D(mm)	Average Weight	Density (kg/ m ³)	External Friction Coefficient	Internal Friction Coefficient
Transparent	40	78.686	2348.11	0.102	/
Blue	25	21.121	2581.64	0.053	/
Green	16	5.744	2678.28	0.104	/

163

164 2.2 Test Programme

165 In the present study, the angle of the flume in laboratory is kept to be 45 degree. **The effect of the**
166 **slope inclination will not be discussed in this paper, but the test results by the authors show that**
167 **the segregation process will basically remain unchanged with different flume inclination. The**
168 **effect of flume inclination can affect the degree of segregation as well as impact forces which will**
169 **be covered by a separate paper later.** Totally 68 laboratory tests have been carried out. The 68 tests
170 are divided into two groups: the first group of tests were conducted on the flume with a small jump,
171 and the other group of tests were carried out on the flume without a jump. Such a jump is also
172 commonly adopted in Hong Kong, and this helps to lower the velocity of the **granular flow** (for
173 small scale flow). Fig 5 shows the flume in laboratory with a small jump. The effects of the particle
174 size and the flowing mass are also studied through the use of balls with different diameter, mass
175 and combination of different balls. Table 2 shows only some of the test programme. Test 1 to test
176 48 belong to the first tests group with a small flume jump. Test 1 to test 6 were carried out by using
177 six different kinds of balls separately with the same mass of 10 kg. The mass of the balls is then
178 changed to 13.55kg and the above tests are repeated again (for test 7 to 10). In order to study the
179 segregation process for test 11 to 40, two kinds of balls with different diameters were combined
180 together, and for the same purpose in test 40 to test 48, three kinds of balls were combined together.
181 Test 49 to test 68 belong to the group without a small flume jump. Same as the first group of tests

182 with a small flume jump, test 49 to test 55 were carried out for same material but different sizes of
 183 balls. In test 56 to test 63, combinations of two kinds of balls were tried. The last five tests were
 184 the combination of three kinds of balls.

185

186 Table 2. Test Programme

Flume with a small jump					
One kind of balls	Test Number		Flow Mass		Balls
	1		10 Kg		G(Transparent)
	2		10 Kg		P(White)
	7		13.55Kg		G(Green)
Two kinds of balls	8		13.55Kg		P(Red)
	Test Number		Top Layer		Bottom Layer
	11		P(White)		P(Red)
Three kinds of balls	26		G(Trans)		P(White)
	Test Number	Top Layer	Middle Layer	Bottom Layer	
	41	P(White)	P(Red)	P(Black)	
	45	G(Trans)	P(Red)	P(Black)	

187

Flume without a small jump					
One kind of balls	Test Number		Flow Mass		Balls
	49		10 Kg		G(Transparent)
	50		10 Kg		G(Blue)
Two kinds of balls	Test Number		Top Layer		Bottom Layer
	55		P(White)		P(Black)
	56		G(Trans)		P(Black)
Three kinds of balls	Test Number	Top Layer	Middle Layer	Bottom Layer	
	67	G(Trans)	P(Red)	P(Black)	
	68	G(Trans)	P(Red)	G(Green)	

188 P: P refers to plastic balls, G: G refers to glass beads

189

190 **2.3 Test procedure and test results**

191 Test materials with different particle size combinations (single type of balls to multiple types of
 192 balls) were put into the container which is on the top of the flume. Figure 7 shows the flow pattern
 193 of single type dry granular material flowing along the flume. The video captured by high speed
 194 camera can show this process clearly. When the gate of the container was pulled up, the front part
 195 of flow mass become loose and start to flow along the upper flume under the action of gravity,
 196 while the latter part of flow mass followed behind. Flow mass elongated when it moved forward,

197 and the shape of flow front is wedge-like type. At the moment when the particles reached the
198 bottom of the flume, the velocity direction of the balls changed because of the angle difference
199 between the upper flume and the lower flume. During the transportation period, a large amount of
200 potential energy of the initial flow mass was transferred to momentum energy accompanying by
201 energy dissipation through the grain collision and friction. Particles at the front of the flow
202 reflected back when they impacted on the wall of deposition zone and collided with the subsequent
203 particles immediately, which consumed the residual momentum energy of flow particles. Finally
204 all the particles rested in the deposition zone.

205 In reality, there are sediments and water in a debris flow. The effect of water is complicated and
206 will not be studied in the present work. The grain size distribution is usually not uniform as in the
207 present laboratory tests. Consequently, a good understanding of the particle flow under a mixture
208 of ball sizes is important. Particle size is a vital parameter for the good understanding of multi-size
209 particle flow because it not only has an effect on the flow dynamic, but also influence the energy
210 attenuation during the whole flow process. **Furthermore**, the tilting test that is mentioned above
211 demonstrates that the dynamic friction angle depends on the particle size, specifically, larger
212 particle size will has smaller dynamic friction angle while smaller particle size will has larger
213 dynamic friction angle. The flow pattern of multi-size particle flow is more complicated **when**
214 compared with the single size particle flow.

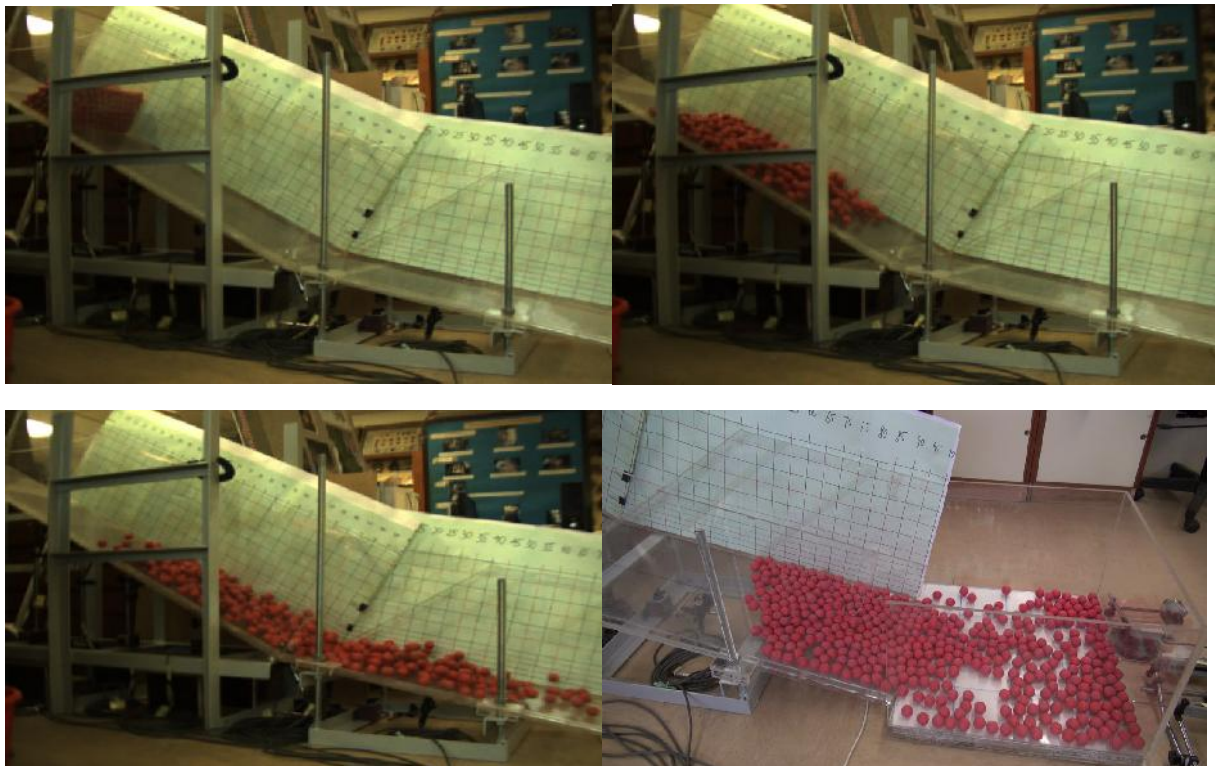
215 Figure 8 shows the flow pattern of multi-size particle flow. Segregation occurred when the
216 combined particles started flowing along the flume. Figure 8a demonstrates the flow pattern of
217 multi-size particle flow composing of white and black plastic balls. The diameter of the white
218 plastic ball is much larger than the black plastic ball as shown in Table 1. From the video captured
219 by the high speed camera, it is easy to observe that during the transportation period, white plastic
220 balls flowed on the upper layer while black plastic balls stayed at the bottom layer. This
221 phenomenon is consistent with the segregation theory of Savage et al. (1988). Besides, it is not
222 difficult to find that white plastic ball always stayed at the front of the flow where the velocity was
223 the highest, in other word, the velocities of the white plastic balls with relative larger diameters
224 are higher than the black plastic balls. Besides, at the upper layer where larger white plastic balls
225 are located, the inertial force dominated the flow dynamic and the energy dissipation was less than
226 that of the lower layer where the flow motion is mainly controlled by the contact forces. For the
227 forgoing reasons, it can be seen that large particle size leads to higher velocity during the flow.

228 Figure 8b shows the flow pattern of multi-size material composing of green glass balls and black
229 plastic balls. The diameter of green glass ball is similar to the diameter of black plastic ball, while
230 the density of green glass ball is almost two times larger than black plastic ball. In the upper
231 container, green glass balls were put statically at the top of the black plastic balls. After pulling up
232 the door, the black plastic balls flowed out firstly at the beginning and stayed at the bottom layer
233 due to the arrangement of the initial position of balls in the container, **and-then** green glass balls
234 quickly moved downwards under the action of gravity, which leads to the **fact-that** green glass
235 balls at the upper layer **were** replaced by black plastic balls subsequently. When the black plastic

236 balls form a stable contact network at the upper layer of the flow, the position transition or
237 segregation process stopped. In this case, the difference of particle sizes between two kinds of balls
238 is not obvious, and segregation was initiated due to the density difference only. During the
239 segregation process in which green glass balls moved downwards and black plastic balls migrated
240 upwards, the momentums of these two kinds of balls were transferred to each other at neighbor
241 location, therefore green glass balls and black plastic balls arrived at the catchment area almost at
242 the same time, while for the test in which balls were arranged in an opposite order (black plastic
243 balls at top and green glass balls at bottom), the green glass balls move faster and deposit earlier
244 at catchment area compared with the black plastic balls due to the smaller dynamic friction angle
245 as well as the larger kinetic energy of the green glass balls.

246 Similar to the above two figures, Figure 7c shows the flow pattern of transparent glass balls and
247 black plastic balls. In this case, both the density and particle size of the transparent glass balls are
248 larger than that of the black plastic balls. As shown in high speed camera video, during the flow
249 process, the transparent glass balls flow upwards and move faster in comparison with the black
250 plastic balls. Hence, although the density of the transparent glass balls is larger than the black
251 plastic balls, the transparent glass balls still stay at the upper layer of the granular flow due to their
252 relatively large particle sizes, which means that particle size has greater contribution for the
253 segregation process than density in the analysis of **granular flow**.

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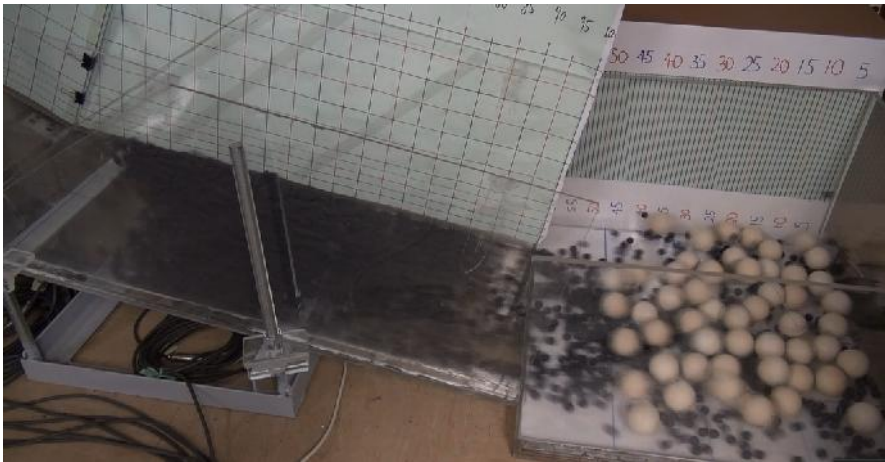


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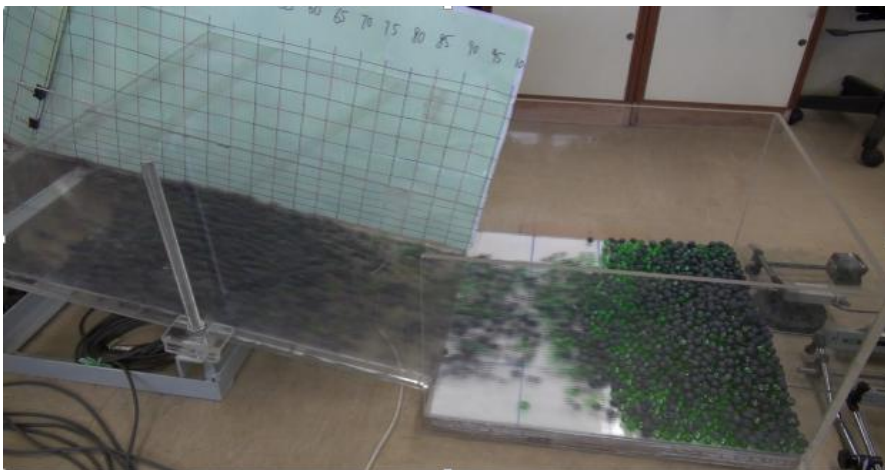
257 Fig. 7. Flow pattern of mono-size particle flow in physical model

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259

260 a) The influence of particle size on segregation process



261

262 b) The influence of density on segregation process



263

264 c) The influence of particle size and density on the segregation process

265 Fig. 8. Flow pattern of multi-size particle flow

266

267 **3. Numerical Modeling of granular flow**

268 **3.1 Model generation**

269 Previous model tests by Chan (2001) for the runout were calibrated by the Dan model, where the
270 problem of segregation and flume jump were not considered. In general, the results are in
271 agreement with those from Rickenmann (in Jackobs and Hungr 2005). For the present studies
272 where multi-size particles are considered, the use of the simple Dan model is insufficient. **The use**
273 **of meshless method to model debris flow has recently been considered by the authors (Wong 2018).**
274 **While the meshless method can give a prediction of the debris flow process, the segregation**
275 **phenomenon is totally neglected in the analysis, but such phenomenon is found to be critical for**
276 **many cases in Hong Kong. In views of the limitations of these numerical methods, the laboratory**
277 **tests in the present study are modelled using the distinct element method,** which is more
278 appropriate for the large deformation, **segregation and separation** phenomenon during the
279 transportation process. Once the appropriate numerical model is established, the numerical
280 technique will be extended to the field tests for which natural sand is adopted. In this paper
281 commercial program PFC2D using DEM has been adopted to implement the numerical simulation
282 of **dry granular flow**. Totally, there are five different methods of model generation in PFC2D
283 program, and based on the consideration of time requirement, the rain method was adopted finally.
284 The parameters used in the numerical simulation are the micro-properties which are difficult to be
285 determined. Benchmark tests have been carried out in order to calibrate the micro-mechanical
286 properties of the dry granular material. Some of the micro-parameters of the balls are determined
287 through changing their values so that the macroscopic behaviors in numerical simulation are
288 consistent with that in physical test. The detailed micro-properties of the balls are shown in Table
289 3. Except for the wall friction (should be small as the walls are relatively smooth) and wall stiffness,
290 all the other parameters in Table 3 are determined by laboratory tests. In order to get different
291 frictional coefficients among the balls, two piece of wood which have plastic balls stick on it
292 regularly and shear force is applied. Furthermore, depositional tests, rebound tests are carried out
293 to measure the frictional angle and rebound coefficients of the balls. For each parameter, five
294 laboratory tests have been carried out, and the mean values are presented in Table 3. It should be
295 noted that there is not a wide distribution in the laboratory determined parameters, hence the range
296 of these parameters are not shown for clarity. The diameters of the particles in the numerical
297 analysis are the same as that used in the physical tests.

298

299 Table 3. Microscopic parameter of the balls for **granular** flow analysis

Balls	Ball stiffness (N/m ²)	Ball damp	Ball density (kg/m ³)	Ball friction	Wall friction	Wall stiffness (N/m ²)
Red plastic ball	2.36e9	0.4	1250	0.462	0.1	1.11e11
Black plastic ball	7e8	0.2	1250	0.1	0.1	1.11e11
Blue glass ball	7e10	0.3	2500	0.1	0.1	1.11e11
Green glass ball	7e10	0.2	2500	0.1	0.1	1.11e11

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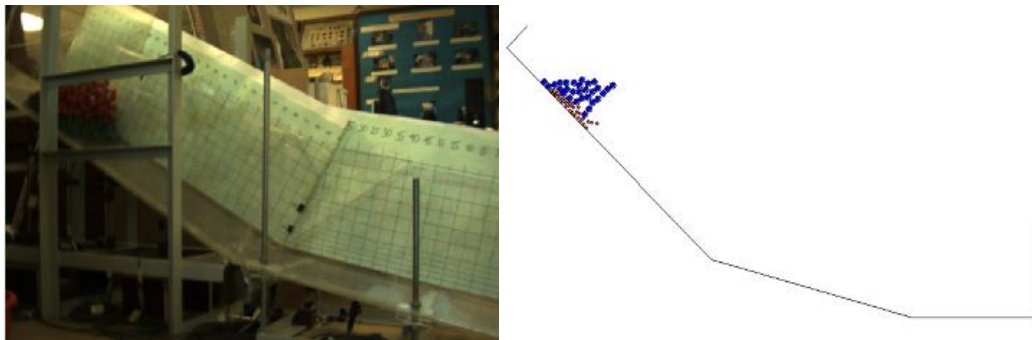
302 3.2 Numerical test results

303 A detailed comparison of the **granular** flow pattern modeled by the physical tests and discrete
304 element analysis is shown in Figure 9. Figure 9a shows the physical test in which both the red
305 plastic balls and green glass balls were used (too many test results are available, and only selected
306 results are used for illustration in this paper). Large blue balls and small red balls in the numerical
307 model represent the actual red plastic balls and green glass balls in the physical model tests
308 respectively. A full-scale numerical simulation is rare to be conducted for discrete element analysis
309 due to the limitation of the computer resource, but this is considered to be necessary and acceptable
310 for the present study. Figure 9b shows the numerical results of the flow pattern of the multi-size
311 particles. Particles start to flow along the flume after the initiation of the flow. During the flow
312 process, the flow mass became longer under the action of shear force. Particles moved apart from
313 each other and pushed other particles forwards. During this process, the momentums of the balls
314 were exchanged and transferred to other balls at the neighbor locations. The flow velocity keep
315 increasing until the front of the flow hit on the wall of the deposition zone. When the kinetic energy
316 of the balls was exhausted, the balls eventually ceased to move at the catchment area. Figure 10
317 shows the flow pattern of multi-size balls flows composing of black plastic balls and green glass
318 balls of which the diameter are relative smaller than the other balls as considered in the present
319 paper. A pronounced Saltation was observed as balls flowed, implying that the collisional character
320 of the flow mass where the savage number is larger than 0.1 (if the savage number is smaller than
321 0.1, the flow belongs to frictional flow, Iverson 1997). Savage number is the ratio between inertial
322 force and frictional force. The comparison between Figure 10 and Figure 9b indicates that the
323 larger the ball size, the more collisional the flow mechanism would be. As a result, the inertial
324 forces dominate the flow dynamic compared with the frictional forces in the present tests.
325 Furthermore, the balls at the upper region of the flow associated with higher velocity had more

326 collisions and moved freely compared with that at the bottom region. The balls at the lower region
327 were compacted with lower flow velocities. By comparison, the numerical simulation results of
328 the flow pattern have a very good agreement with the physical test results when the micro-
329 parameters were selected suitably.

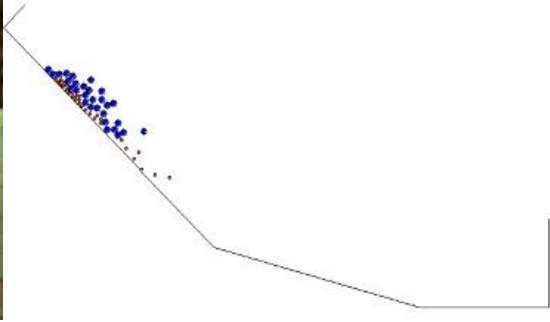
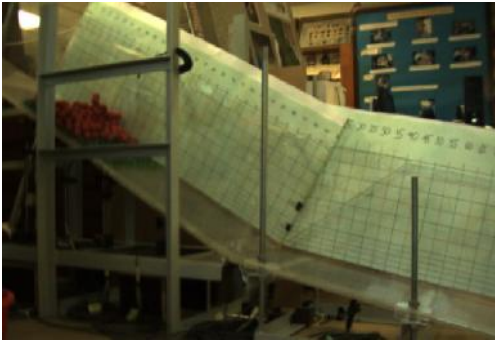
330 As shown in Figure 9b and Figure 10, segregation was also observed in the numerical model after
331 the dry granular balls started to move. In Figure 9b, it was evident that the blue balls with larger
332 ball size moved upwards and forwards, while the red balls with smaller ball size went to the lower
333 layer and stayed at the rear of the flow, which was consistent with the results in the physical model
334 tests. Smaller particles are more likely to move through the void between the larger particles, and
335 this will in turn squeeze the large particles to the upper layer of the flow. Because of the momentum
336 exchange between the balls and the flow mass dilation resulting from the shear deformation, a
337 dispersive pressure was caused which result in larger dry granular balls moved faster than the finer
338 particles and went upwards, and lead to the results that larger balls flowed to the upper layers
339 where the shear strain is low and accumulated at the front of the flow, while the finer balls tend to
340 moved downwards and accumulated at the bottom of the flow (Takahashi (1981)). Besides, the
341 difference of the ball size induce an unbalance forces on the balls which restrict the vertical
342 movement of the balls, this will also affects the flow segregation in the vertical direction.
343 **Furthermore**, the density difference between the balls the in numerical model is another factor that
344 influence the segregation process. Particles with lower density are more likely to rise to the free
345 surface while particles with higher density are more likely to segregate to the bottom of the flow.
346 From Figure 5b, it can be noticed that it is easily for the red balls with larger density traveled
347 through the gap generated by the shear deformation and squeezed the particle with smaller density
348 up to the upper flowing layer. The balls with higher density at the bottom pushed the balls with
349 smaller density forward. It is worth to mention that from the simulation results, the velocities of
350 the blue balls at free surface is the largest, which result in that the balls with large size migrated to
351 the front of the flow. The segregation mechanism simulated in the numerical model is in consistent
352 with what is aforementioned in the physical model tests. Ashwood and Hungr (2016), Choi et al.
353 (2014), Choi et al. (2015), Kwan (2012), Lo (2000), Ng et al. (2014), Ng et al. (2017) **have**
354 investigated the impact forces on the barrier which is however not considered in the present study,
355 **as this is not the main theme of the present work.**

356

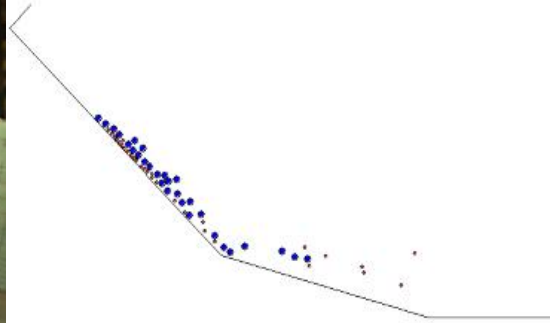
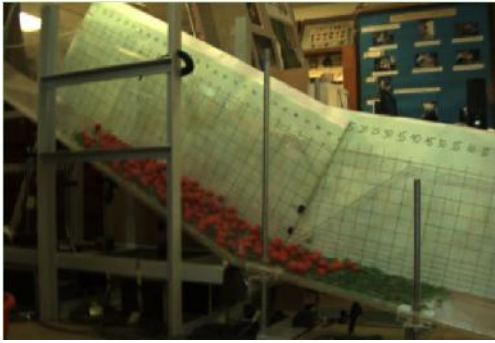


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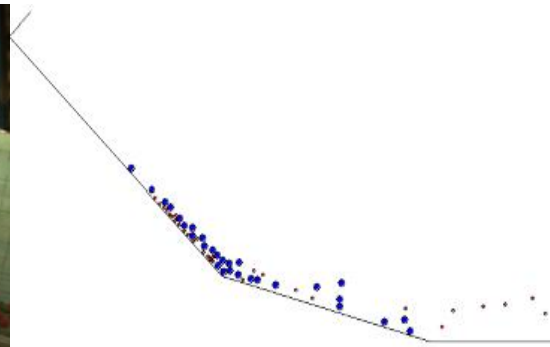
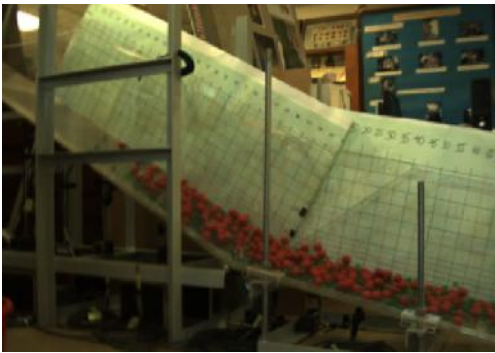
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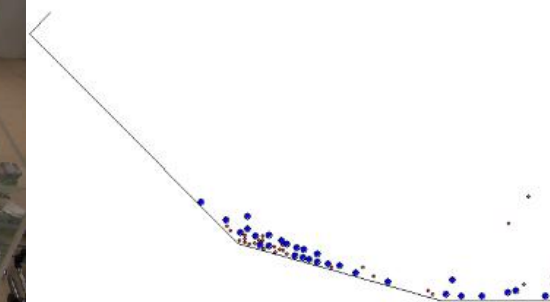
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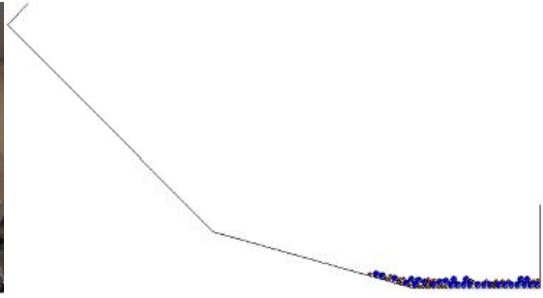
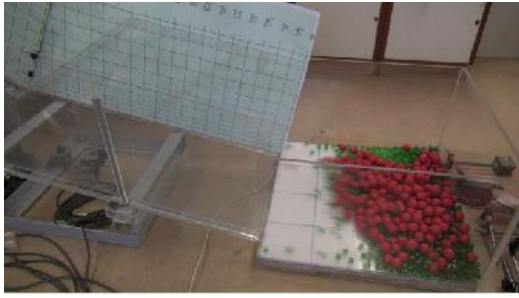


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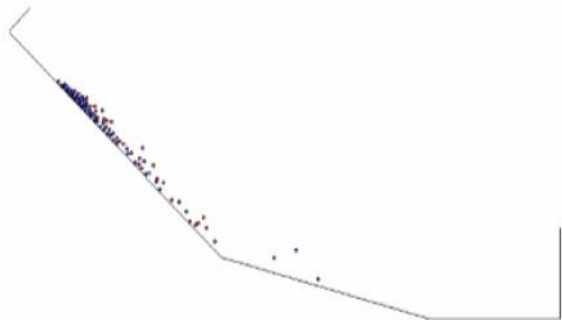
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363 Fig. 9a. Flow pattern of multi-size
364 balls flow in physical test

363 Fig. 9. Flow pattern of multi-size
364 balls flow in numerical test

365 Fig. 9. Flow Pattern of multi-size particle flow composing of red plastic balls and green glass
366 balls

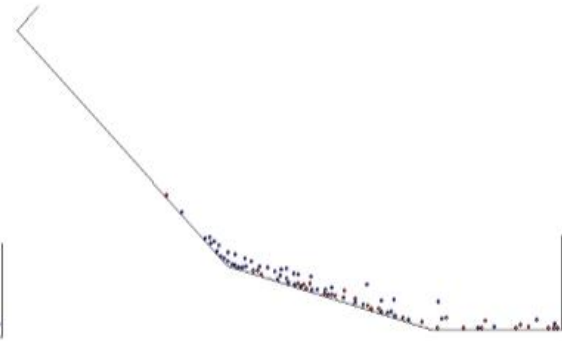
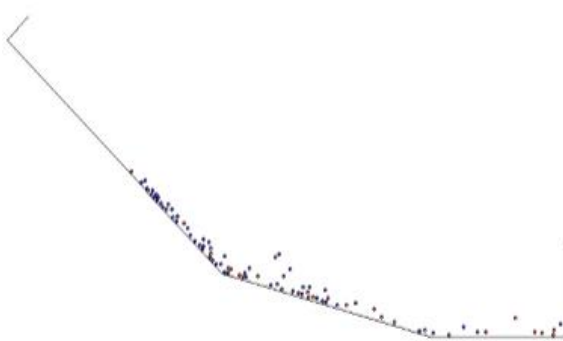
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368

369 (a) Start of flow

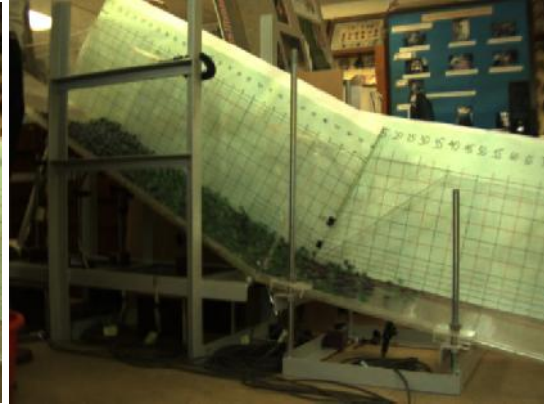
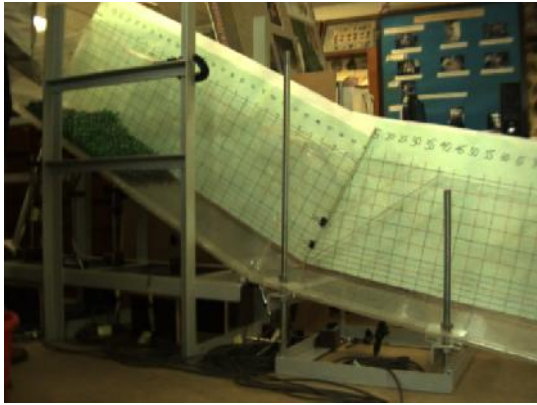
(b) 1/3 of flow time



370

371 (b) 2/3 of flow time

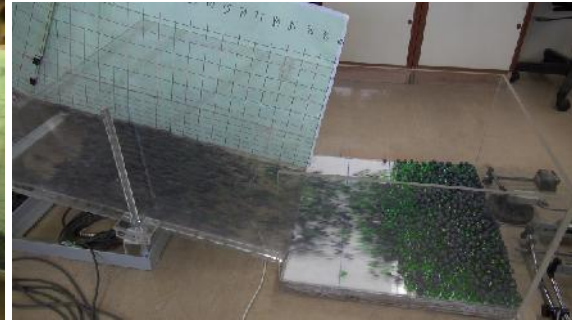
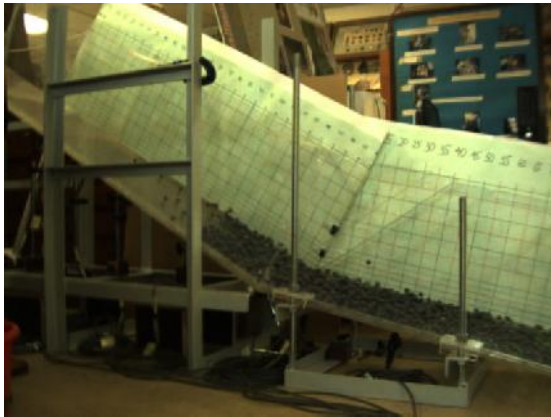
(d) end of flow



372

373 (e) Photo at start of flow

(f) photo at 1/3 of flow time



374

375 (g) photo at 2/3 of flow time

(h) photo at final stage

376

377

378 Figure 10. Flow Pattern of multi-size particle flow composing of black plastic
379 balls and green glass balls

380

380 3.3 The effect of the flume jump

381

382 To reduce the impact force and velocity of the granular flow mass, the authors have proposed to
383 add a jump in the flume as a pilot test in this study. From the results in this study, it is found that
384 the construction of a jump which has a very low cost has some small advantage in reducing the
385 impact from debris flow. Based on the present result, some rigid barriers in Hong Kong have
386 started to include a jump as a small benefit to the control of debris flow, and this is the reason for
387 carrying out such a test in the present research programme which is seldom considered in the past.

388

389 Figure 11 shows the numerical results of the flow pattern of the blue glass balls flowing on the
flume with or without a jump. The flow pattern of the blue glass balls flowing on the flume without
a jump in the numerical model is almost the same as the flow pattern of the red plastic balls in the

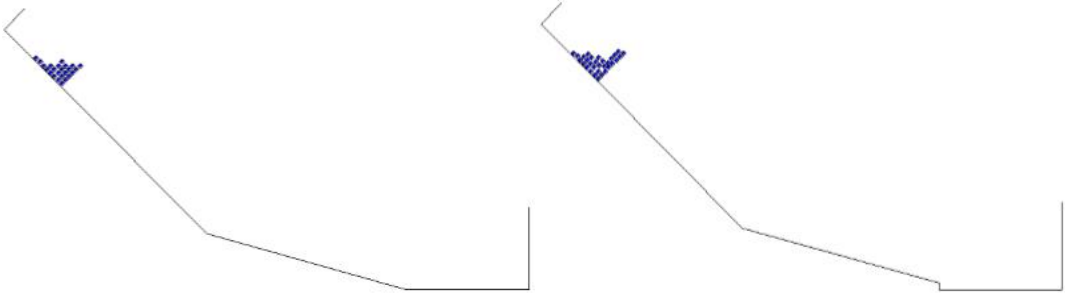
390 physical tests aforementioned. From the comparison of the flow pattern between Figure 11a and
391 Figure 11b, an important phenomenon was observed. The run up height of the balls flowing on the
392 flume with a jump is obviously lower than the run up height of the particles flowing on the flume
393 without a jump, which indicates that flume jump is able to facilitate the process of energy
394 attenuation and thereby has a good effect on suppressing the run up height of **granular flow**.

395 Figure 12 exhibits the velocity of the blue glass balls at different time step. In PFC2D, we have
396 developed the code to monitor the maximum velocity of the balls for comparison purpose, and the
397 monitored results are used to produce Fig.12. Black line represent the maximum velocity of the
398 blue glass balls with 10Kg weight flowing on the flume without a jump at different time step, while
399 the red line represent the same kind of balls with 13.55Kg weight on the flume with a jump. The
400 comparison of the velocities at point A and point B indicates that the peak velocity of the balls
401 flowing on the flume with a jump is pronouncedly smaller than that on the flume without a jump,
402 and the peak speeds of the balls on the flume with a jump were achieved earlier than balls on the
403 flume without a jump. It is worth to mention that the velocity of the balls is independent of the
404 mass of the test material, except that at the peak period.

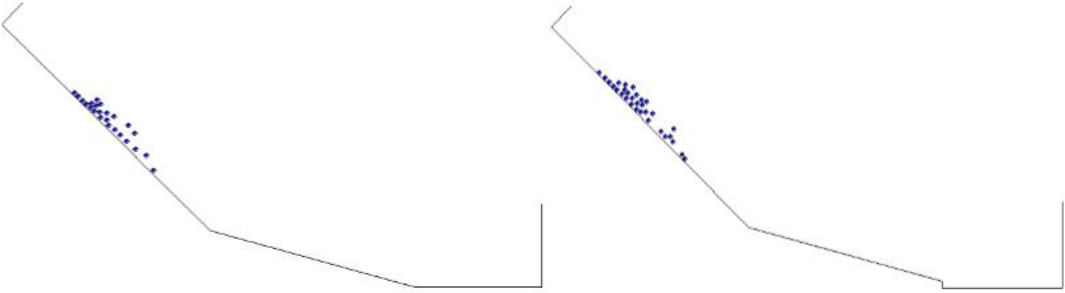
405 Figure 13 shows the velocity profile of mono-size particles (blue glass balls) along the flume with
406 or without a flume jump. The length of the velocity vector represents the speed of the particles.
407 From Figure 13, it can be noticed that the front flow velocities are the largest compared with the
408 velocities of the particles at the rear of the flow. When these particles approached the lower part
409 of the flume, the velocity directions changed due to the difference of the flume angles. This is in
410 good agreement with the laboratory results mentioned above. Figure 13b shows that the velocity
411 of mono-size particles on the flume with a jump increased after the initial state. The largest flow
412 velocity was achieved at the moment when these particles intend to jump into the deposition zone.
413 The directions of flow velocities changed and the speed of particles decrease as soon as they fell
414 into the deposition zone. As with those particles moving on the flume with a jump, the velocity of
415 the particles flowing along the flume without a jump increased when they approached the
416 deposition zone, however, the velocity of these particles kept increasing when they flowed into the
417 deposition area and the peak speed was achieved just before the moment when they reached the
418 boundary of the deposition area. When the granular front impacted on the wall of the deposition
419 area, these particles at the front of the flow reflect back and collide with the following particles,
420 and that is the moment when the flow speed decelerated.

421 According to Figure 12 and 13, the peak velocity of the balls on the flume with a jump achieved
422 before they impacted on the wall of deposition zone compared with that without a jump, which is
423 meaningful to the engineers because the flume jump can effectively reduce the impact force on the
424 barrier. Besides, the jump of the flume is capable of reducing the peak velocity of the dry granular
425 particle flow as well. **To sum up, flume jump plays a useful role** in attenuating granular flow,
426 therefore, flume jump is recommended to be applied in the design of debris flow barrier (which is
427 actually sometimes adopted in Hong Kong).

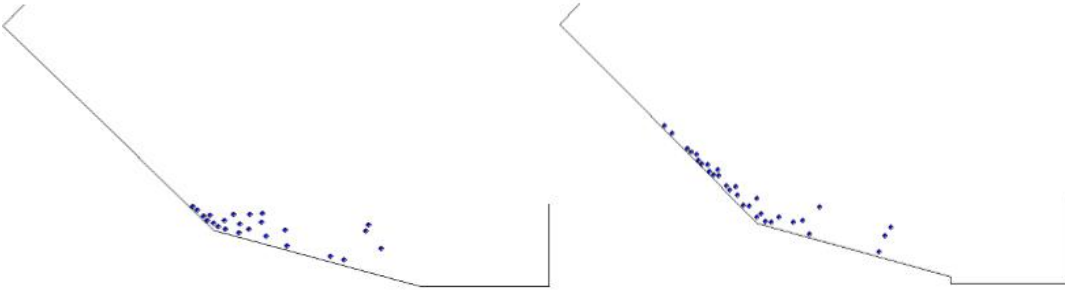
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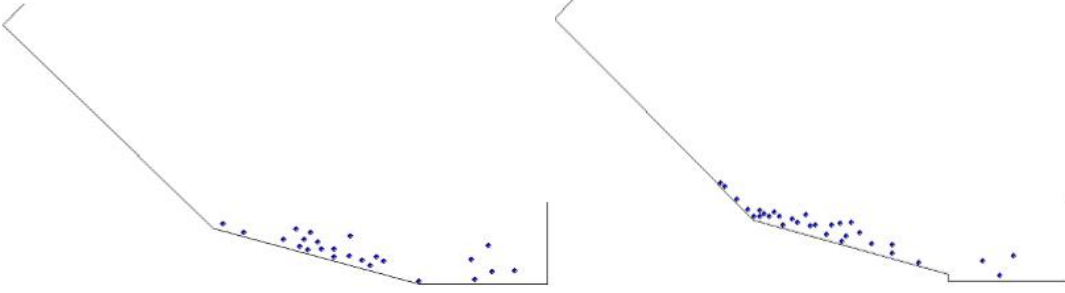
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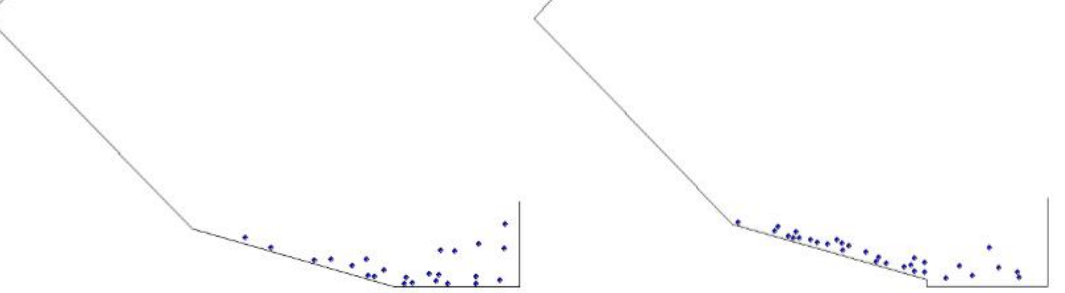
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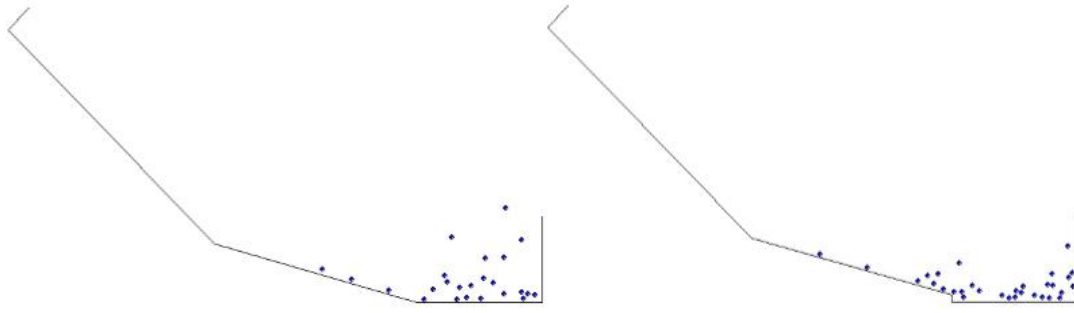


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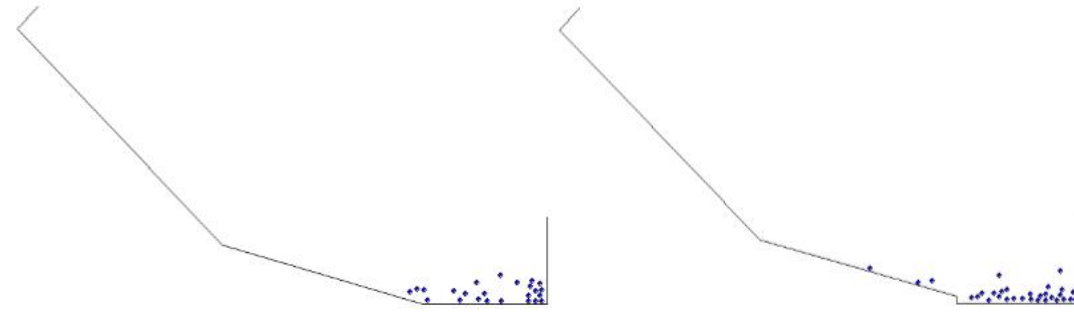


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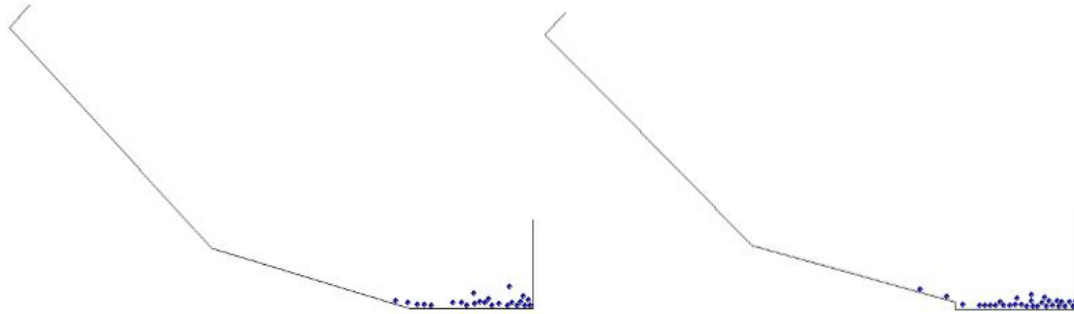
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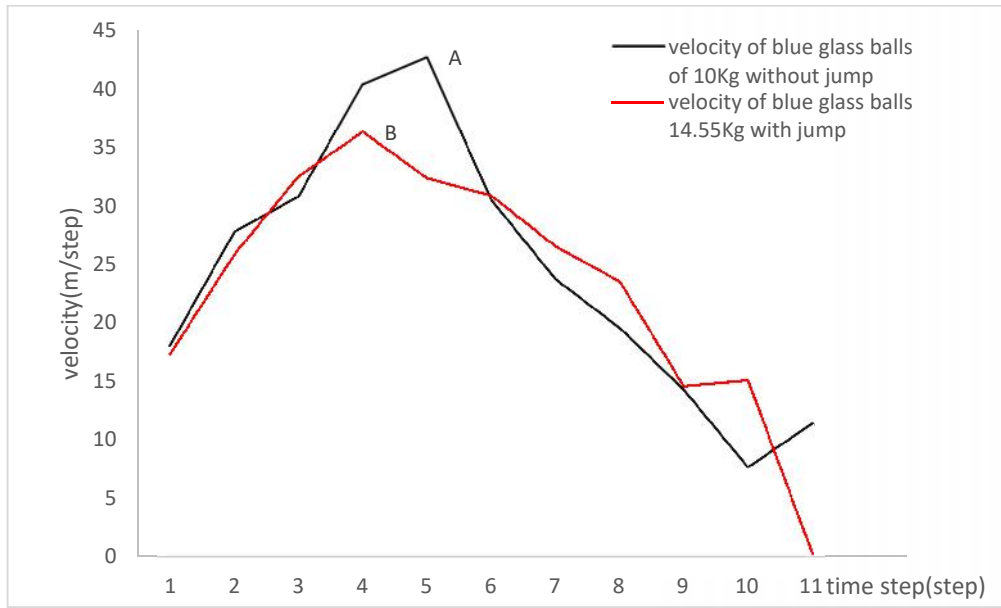


437 Fig. 11a. Flow pattern of blue glass balls
438 flowing along the flume without jump

437 Fig. 11b. Flow pattern of blue glass balls
438 flowing along the flume with jump

439 Fig. 11. Flow pattern of blue glass balls flowing on the flume with or without a jump

440



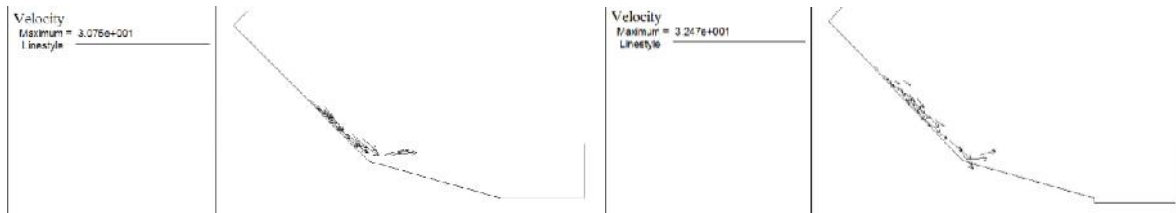
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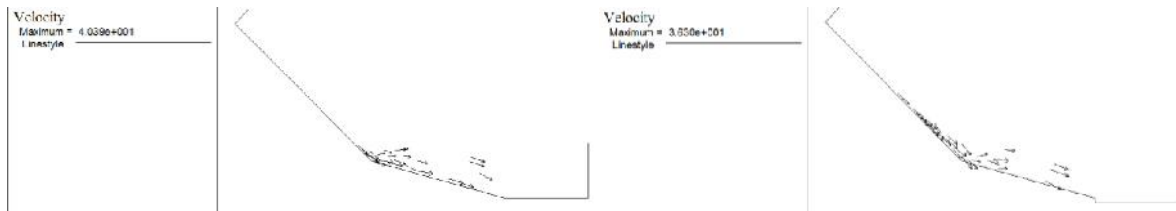
Fig. 12. Maximum velocity of blue glass balls in numerical model

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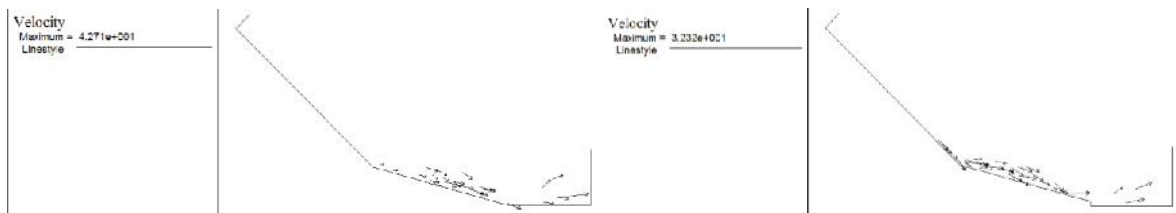
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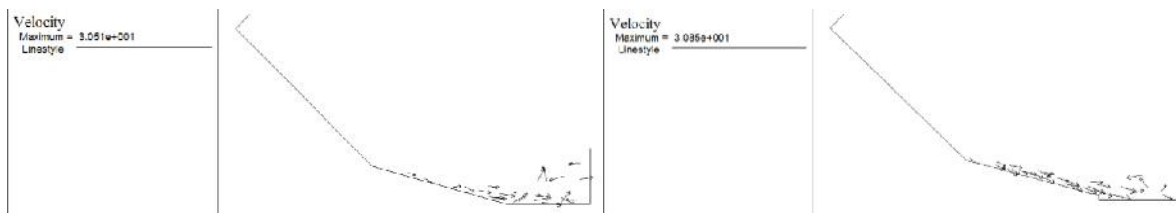
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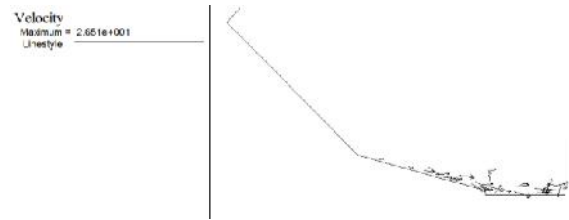
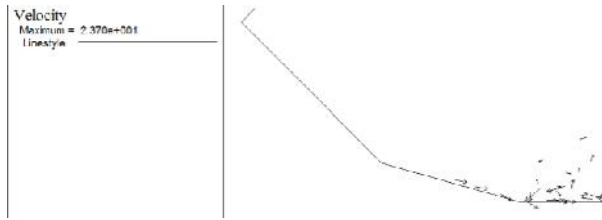


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451

452

Fig. 13a. Velocity profile of balls on the flume without a jump Fig. 13b. Velocity profile of balls on the flume with jump

Fig. 13. Velocity profile of blue glass balls in numerical model

453 It should be **noted** that the actual flow velocity of the balls can be traced back from the high speed
 454 camera photos and the movie, but we do not present the results here because it is not the main
 455 theme of the present study. Most importantly, ~~this is due to the limitations of~~ DEM usually cannot
 456 give a good ~~for which~~ quantitative prediction ~~analysis is usually not good~~ unless the micro-
 457 parameters are fine tuned. The authors do not prefer such tuning of the parameters, as such tuning
 458 cannot be performed **before** the tests. However, the qualitative results from the DEM analysis and
 459 the laboratory tests are reasonable **as found from the present study**, hence we can still accept the
 460 results from DEM in our discussion. Actually, the authors have carried out limited tuning of the
 461 micro-parameters (**not shown in this paper**) in our internal studies. Since the flow and segregation
 462 process are practically not affected by the change of **these micro**-parameters (but the actual value
 463 of the flow velocity, run-out ... are affected), we have not included these results in the present
 464 paper, and the authors prefer to concentrate on the segregation and jump for **with** a flume **test**.

465

466 5. Large scale field tests

467 After the laboratory studies using a 1.5m long flume and glass/rubber balls, the authors have
 468 carried out a large scale flume test which is shown in Fig.14. The flume is about 6m long, and 5
 469 types of sand as shown in Fig. 15 are used in the field tests. The particle size within each type is
 470 relatively uniform, and they ranged from 1-3mm, 3-5mm, 5-7mm, 7-8mm and above 8mm. The
 471 friction angles for the 5 types of sand as determined from the deposition tests as shown in Fig.15b
 472 are given by 28°, 30.3°, 29.1°, 31.5° and 33.7° respectively.



473

474 Fig.14 Large scale flume for field test



475

476 Fig.15a Sand used for granular flow tests



477 Fig.15b Deposition tests for sand

478

479 A series of tests with single, double and triple types of sand have been carried out, and only some
480 of the results are shown in this paper for comparisons with the laboratory tests. As shown in Fig.16,
481 the final deposition profile using type 1 (1-3mm) and type 4 (7-8mm) sands is shown. It is noticed
482 that the coarse grain sand move to the top of the flow, which are illustrated by Fig.17a to 17c. Such
483 results comply well with the laboratory studies. The control tests using coarse and finer sands are
484 shown in Fig.18. A closer look into the difference between Fig. 18a and Fig.16 is the profile at the
485 rear can reveal an important difference. For granular flow with 2 types of materials, the difference
486 in the height of deposit for the first meter as measured from the left is greater than that for the test
487 with single material (true for all single sand tests). Such phenomenon can be attributed to the effect
488 of the difference in the velocity flow between type 1 and 4 material, and type 1 material deposit at
489 the bottom during the flow. Based on the field tests, the importance of the particle size during the
segregation process as derived from the laboratory tests can be further verified.

490



491

492 Fig.16 Final deposition after the granular flow for two materials (coarse and fine)



493

494 Fig.17 a Deposition at the rear of the deposit



Fig.17b Deposition at the front of the deposit

495



496

497 Fig.17c Front view of the deposition (2 materials)

498



499

500 Fig.18a Front view of the deposition (type 4 material) Fig.18b Close up view of the deposition

501

502 With reference to Fig.19, it is clear that the formation of the flow front, flow head, channelized
503 flow and levee from the present field test is very similar to that by Johnson et al. (2012). The
504 surface trajectories of the particles by Johnson et al. (2012) are also captured by the high speed
505 camera in the present laboratory and field tests. A coarse enriched surface layer has been obtained
506 by Johnson et al. (2012), and such phenomena are also obtained from the laboratory and field tests
507 and is clearly illustrated in Fig.17. Iverson (1997) has also found similar segregation from the

508 granular flow at Oregon (1996). It should be noted that for all the granular flow tests in the present
509 study, such segregation phenomenon is always obtained, as long as there are more than 1 materials
510 in the problems.



511
512 Fig.19 Front of the runout

513 6. Discussion

514 Laboratory tests were carried with numerical simulations through distinct element method to study
515 the flow pattern of dry granular flow. The study is important for the basic understanding of the
516 granular flow segregation problem and the importance of providing a jump in the flume ~~or~~ in the
517 actual protective measures. For the present tests, the flume base is even and smooth which result
518 in relative small dynamic frictional angle and less energy attenuation compared with the real
519 granular flow. Besides, the surfaces of the glass and plastic balls used in the experiments are
520 regular and smooth, while for debris flow occurring in nature, the debris materials are always
521 irregular and rough, which cause the dynamic internal frictional shear force between real scale
522 debris flow particles ~~are~~ relatively large with a lower ~~and hence the~~ run up height ~~is lower~~. As a
523 consequence, ~~the present tests is a conservative test~~ to study the flow pattern of granular flow.
524 Such arrangement is necessary ~~so as to separate the contribution of particle size distribution from~~
525 ~~other parameters in the segregation process.~~

526

527 Physical tests were conducted to study the flow pattern of mono as well as multiple size particle
528 flows. In general, the results from the present study comply well with those from the literature.
529 Test results indicate that flow mass elongated under the action of shear force during the particles
530 flowed on the flume. For multi-size particles with different particle sizes, segregation always
531 occurs. Particles with larger diameters migrated upward and small particles moved downwards

532 because particles with smaller diameter can go through the gap between the larger particles. In
533 addition, the density of the particle is another factor that play a role in the segregation process.
534 Under the action of gravity, particles with higher density moved downwards faster and other
535 particles with lower density were squeezed up. For the real scale debris flow, the debris material
536 ranges from clay and silt to boulders while the differences in the densities between different types
537 of particles are relatively small, hence particles size will be the most dominant factor which
538 influence the segregation process. **The top view** from high speed camera indicates that the
539 velocities of the large particles are higher than the velocities of the small particles. Granular
540 particles with larger particles sizes travelled to the front of the flow where the velocities are higher.
541 Larger particle size is observed to lead to a higher velocity. Such results are also in general
542 agreement with the results by Takahashi (1980).

543

544 **For the present work, the detailed movement of individual particle is hard to trace even with the**
545 **help of high speed camera. Instead of that, the authors choose to trace the segregation process**
546 **through the macro phenomena such as grain migration, segregation and the formation of the levee.**
547 **Combined with the DEM analysis, the interpretation of individual grain movement as well as the**
548 **formation of the segregation and levee can be assessed. Based on the various laboratory and field**
549 **tests on flow with mixture of different material sizes, stiffness and density, it is established that**
550 **the grain size distribution is the most critical factor in the flow process, as grain movement occur**
551 **and control the flow process at about half of the flow process. The formation of the force chain**
552 **which actually affect the flow process is also controlled by the grain size distribution. This result**
553 **has an important implication in that most of the natural flow process involve debris of different**
554 **grain sizes.**

555

556 For the flow pattern of dry granular particles simulated through distinct element method, the
557 simulation results of flow pattern are almost the same as the physical tests. Berger (2016), Chen
558 and Lee (2000), Ghilardi et al. (2001) also obtained a reasonably well numerical modeling of the
559 flow process for relatively simple flow problem which support the use of numerical analysis for
560 the **granular flow** problem. In the present numerical model, a pronounced segregation process was
561 observed as well, which comply well with many previous studies by Gray et al. (2003),
562 Hákonardóttir et al. (2003), Iverson (1997), Johnson et al. (2012) and many others. Large particles
563 went upwards while small particles went downwards. From the velocity vector figure, the
564 velocities of the particles at upper layer as well as the velocities at the front of the flow were the
565 largest. Savage numbers of the dry granular particles in present tests were larger than 0.1, which
566 represent the collisional character of the flow. The flow behavior was hence more inertial than
567 frictional. Flume jump have a significant influence on the impeding **granular flow**. When the
568 particles flowed through the jump a large quantity of kinetic energy were consumed during this
569 process. The peak velocities of particles flowing on the flume with a jump were lower than that
570 without a flume jump. Besides, the peak velocities of the particles on the flume with a jump were
571 achieved earlier, and after that the flow velocity started to decrease, which would make a great
572 contribution for reducing the impact load. The run up height of the particles on the flume with a

573 jump was apparently lower than that without a jump. Thus, flume jump can help to reduce the flow
574 velocity as well as suppress the run up height. In previous sections, detailed discussion about the
575 formation of force chain from DEM are investigated, and such force chain has a major effect to
576 the flow and segregation process which is actually observed from the tests. Without the DEM
577 results, these phenomenon cannot be explained clearly. In this respect, the use of numerical
578 modelling has provided an important help to the understanding of the flow and segregation process.

579 Comparing the physical and numerical test results, the macroscopic flow behavior in numerical
580 models are consistent with the physical tests. Through a good selection of the model generation
581 method and micro parameters, the distinct element method can produce a reasonable qualitative
582 simulation of the behavior of dry granular flow for the consideration of the engineers. These results
583 have useful contributions to the better understanding of the granular flow behavior which is not
584 possible for the other classical methods. Up to the present, the engineers are still relying on some
585 empirical methods such as dynamic impact earth pressure coefficient (Kwan 2012) or similar
586 approaches for the design of flexible or rigid barrier, as granular flow process is complicated by
587 many geotechnical and geographical complexities. The design of the barrier is still more an art
588 than science up to the present, though some guidelines are available to help the engineers in the
589 design. ~~Distinct element analysis is well known to be more suitable for qualitative than quantitative
590 description. It is possible to tune the parameters so as to give quantitative matching, but this is not
591 the purpose of the present work. Without test measurement, such matching is not possible. The
592 purpose of the present work is to demonstrate the general applicability of the distinct element
593 modelling in dry granular flow problem. For the tuning of the parameters to give quantitative
594 comparisons, this is trivial and will not be discussed here, as this is not the main theme of the
595 present work. So far, quantitative study using DEM is still difficult, due to various difficulties in
596 micro parameters determination, contact model and other factors. These limitations are well
597 known, and up to now are still open questions. The focus of the present paper is the segregation
598 process from a qualitatively assessment, and the authors are also working on the possibility of
599 quantitative DEM assessment so as to compare the computed results with the actual laboratory and
600 field tests results on velocity of parameters and other information. However, The DEM analysis in
601 this study can supplement the field and laboratory studies for which the internal forces between
602 the particles cannot be determined. instead being the main theme of the present work, hence no
603 detailed comparisons between the results from tests and DEM analysis is carried out. Some tuning
604 of the micro parameters have been carried out (not shown), but the overall behavior is practically
605 not affected, as the segregation process is largely controlled by the particle size.~~

606

607 The flow process and segregation process from laboratory and field tests are similar in many
608 respect – largely controlled by the particle size distribution. This is clearly illustrated from about
609 50 tests in our study. Limited photos are shown in this paper to limit the length of the paper.
610 Thousands of photos and about a hundred movie files are obtained from the laboratory and field
611 tests in this study, and only selected photos which are sufficient to illustrate the main purposes of
612 the present work are shown in the present paper. The authors are however happy to share these
613 materials upon request at cymchen@polyu.edu.hk.

614

615 In the present paper, the effect of the flume inclination has not been investigated. Actually, the
616 authors have carried out some tests on the effects of flume inclination. For the segregation process,
617 the test results indicate that the basic conclusions from the present work remains unchanged, for
618 practical purposes. Flume inclination has more important effects on the impact forces and erosion
619 which are to be covered by the next stage of the present research work.

620

621 7. Conclusion

622 In the present study, two important phenomena in **granular flow** are studied. The first problem is
623 the segregation process which is captured in all the tests in the present studies. The segregation
624 phenomenon can affect the design of the barrier in different ways. The finer materials will be
625 deposited at the bottom of the runout, and the relatively lower permeability of this layer will tend
626 to drive the water level upward (somewhat similar to the perch water table phenomenon). This
627 may increase the destructive power of water. For the design of rigid barrier, the use of a suitable
628 water table will also be crucial to maintain adequate factor of safety of the barrier. Since
629 segregation will occur practically for majority of the debris flow problems, this effect should be
630 well studied and considered in the design of flexible and rigid barriers.

631

632 The authors have chosen flexible spherical rubber beads as well as rigid glass beads for the
633 laboratory, and the range of stiffness would be sufficient to cover most of the natural flow materials.
634 The segregation process as found from the laboratory test is actually similar to that in the field
635 tests using non-spherical sand. Through such selection, it is clearly demonstrated that particle size
636 distribution is a very critical factor in the segregation process, and it appears that it is more critical
637 than particle shape or stiffness.

638

639 To reduce the destructive power of the debris, a small jump in the flow channel is sometimes
640 applied in Hong Kong if the site condition allow. In general, the effect of this jump is small, and
641 is effective only for small volume debris flow which is the common case for Hong Kong.
642 Nevertheless, such provision can slightly reduce the destructive power of the debris. It is
643 interesting to note that there is virtually no study about the effect of the jump in the past, and the
644 present work provide some useful pilot works, for which more works may come out in the future.

645

646 One of the main limitations for the present study is that the flow material is limited to granular but
647 not cohesive material. The reason is that all debris flows in Hong Kong are practically granular
648 debris flows. The most critical factors in debris flow for Hong Kong include also different particle
649 size distribution (studied in the present work), topography and the effects of water. The present
650 work do not aim to consider all these effects simultaneously, but is confined to address the critical

651 issues as found in Hong Kong. Nevertheless, the present work will still be useful to many countries
652 where the flow material is mainly granular.

653

654 The authors are currently considering the next stage of field tests, for which the wet test will be
655 carried out (~~limited tests have been so far~~), and more equipment and measurements will also be
656 used. ~~There are however some practical considerations which include time, money, and the setup~~
657 ~~of the test materials and other factors.~~ Currently, the authors are constructing a laboratory flume
658 where the base is rough. The combined effect of base roughness and flume inclination angle will
659 be carried out soon, and hopefully the results will form the extension of the present paper. For the
660 field test, most of the researchers place a contained of wet sample and let the sample flow down.
661 This approach is simple to be executed, but the actual debris flow may not be like that. From the
662 observations of several debris flows in Hong Kong, the authors have noticed that erosion process
663 is ~~sometimes an important phenomenon which is not simple~~ to be reproduced in the field flume.
664 The composition of the flow material actually changes during the flow process. More thoughts will
665 be given to the setup of the wet field test in the future, and the base of the flume may be specially
666 prepared with some soil bedding to allow for erosion in the future tests.

667

668 **Acknowledgement**

669 The present project is funded from the Research Grants Council of the Hong Kong SAR
670 Government through the project PolyU 152293/16E, and CityU University of Hong Kong
671 Research Project No. 7004631, National Natural Science Foundation of China (Grant No.
672 51778313) and Cooperative Innovation Center of Engineering Construction and Safety in
673 Shangdong Blue Economic Zone.

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Suggestions for revision or reasons for rejection (will be published if the paper is accepted for final publication)

The revision shows significant improvements in terms of technical content and clear presentation. Following comments shall be handled properly before it is accepted for publication.

1. In the response, the authors stated the wet tests were not performed due to the limitations of budget and time. Because the title has been changed, the content related to debris flow shall be changed accordingly. – The content has been greatly revised to reflect that the main theme is granular flow, which is a special case of debris flow. I have also used the term debris flow and granular flow carefully in the revised manuscript to reflect more precisely the works as discussed.
2. The caption of Fig. 2 is associated with slope stability analysis. However, the plot only shows the mesh. It shall be removed because it is not related to the "debris flow". I have added Fig.2b and some discussion to show the debris flow after the slope failure, to illustrate the relation between slope stability and debris flow, from engineer's view.
3. All the reviewers mentioned that in-depth analysis and discussions shall be presented. The authors shall address this issue and/or focus on the available findings. More discussion has been added to reflect the findings.
4. It is inadequate to copy the responses on the revision. The revised content shall meet the technical writing format and style. – Not all comments are copied and responded in the revised manuscript. I try to avoid this actually. Only those comments and responds which are useful to the reading and illustration of the paper are included in the revised manuscript. I have further revised the manuscript to improve the technical writing format. Some replies which are not that relevant to the paper are removed.
5. Section 3.3 is Irrelevant to the title. The authors shall explain or describe why this is included in the manuscript. – This is important in that a jump in the flume and the debris flow channel can help to reduce the impact force from the debris flow, which is seldom considered in the past. This has been found to be useful in Hong Kong, and this is now used in some of the rigid debris flow barrier in Hong Kong. This is further explained in the revised manuscript.

Furthermore, I have made various corrections and improvements to the use of English in the revised manuscript.

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